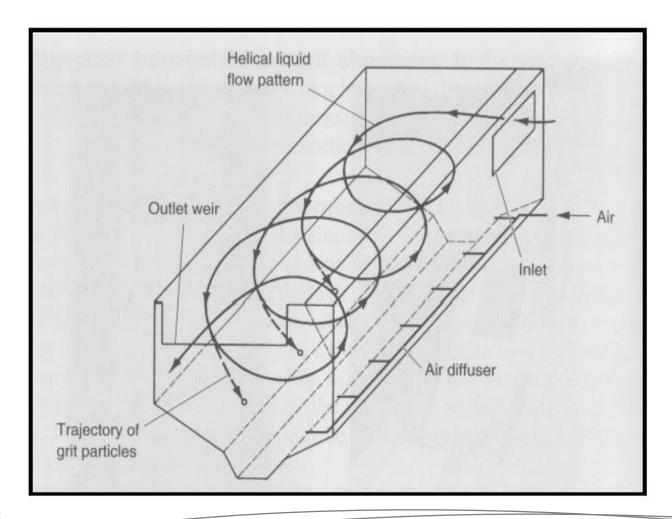
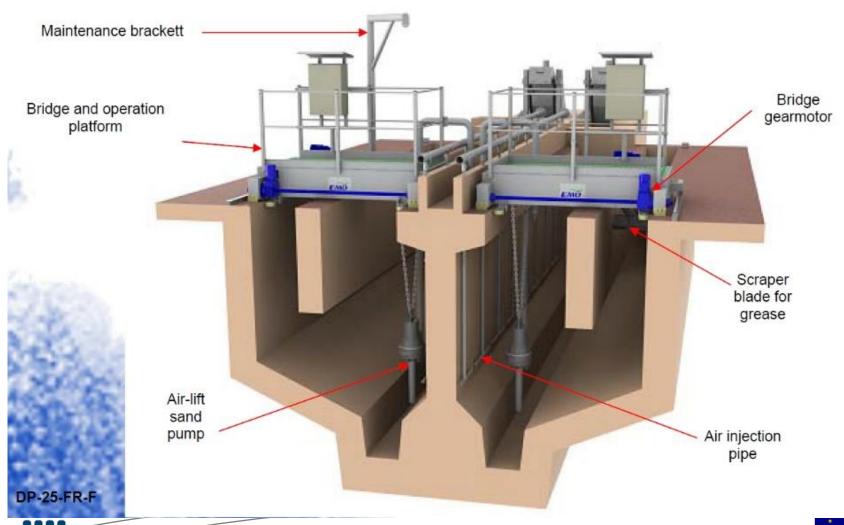
HELICAL FLOW PATTERN IN AERATED GRIT CHAMBERS



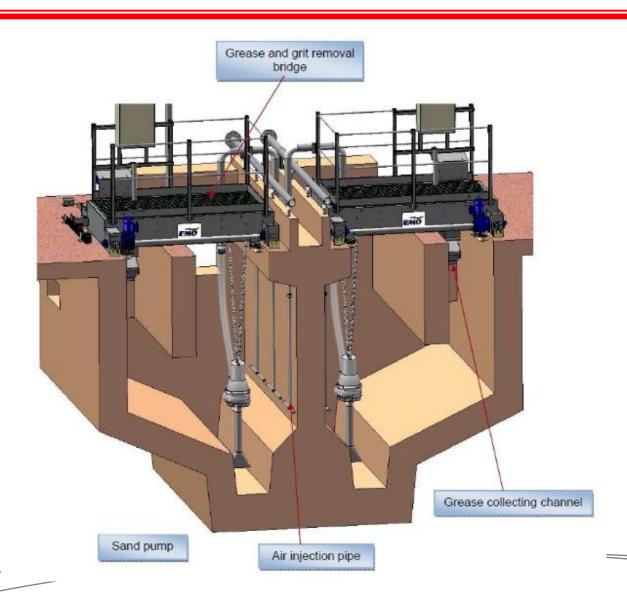




AERATED GRIT CHAMBERS WITH AIR LIFT PUMPS

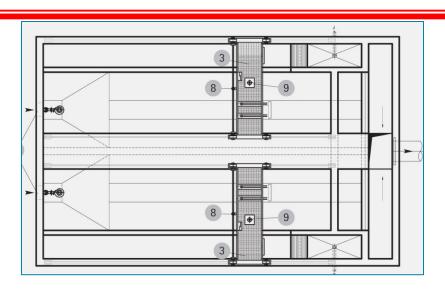


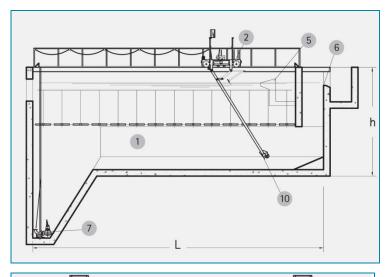
AERATED GRIT CHAMBERS WITH GRIT PUMPS





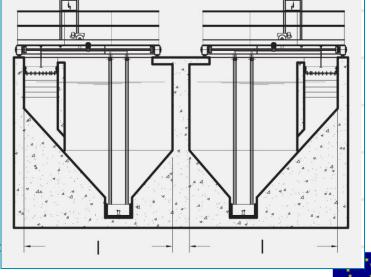
AERATED GRIT CHAMBER WITH HOPPER







CONSULTANTS



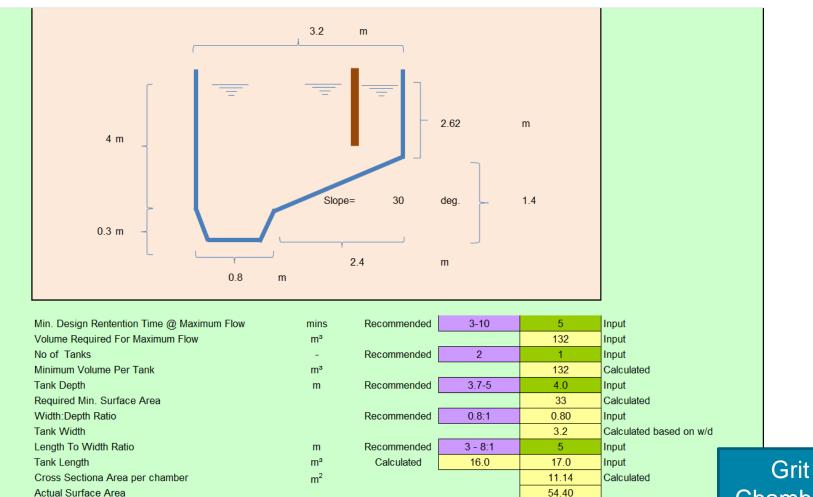
TYPICAL DESIGN PARAMETERS FOR AERATED GRIT CHAMBERS

Item	Unit	Range	Typical	Source
Min. detention time at peak flow rate	min	3-10	5	MOP-8
Depth	m	3.7-5		MOP-8
Length	m	7.5-20		M&E
Width	m	2.5-7		M&E
Width-depth ratio		0.8-1		MOP-8
Length-width ratio		3-8 to 1	4:1	MOP-8
Air supply	m3/m.min	0.2-0.5		M&E
Grit quantities	m3/10^6 m3	4-200	15	M&E





EXAMPLE GRIT CHAMBER DESIGN



28.7

57.4

m³

m³

mins

189.4

189.4 7.2 Calculated

Calculated

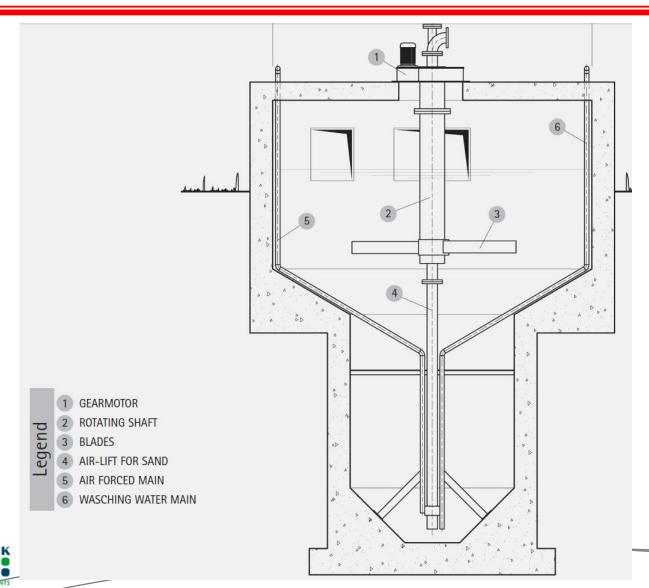
Calculated

Actual Total Volume

Actual Retention Time

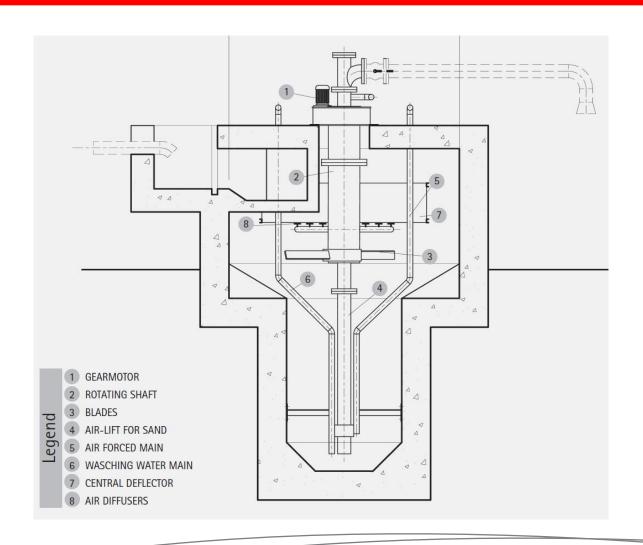
Actual Volume per chamber

ROTATING BLADES GRIT REMOVAL





ROTATING BLADES GRIT REMOVAL WITH OIL REMOVAL







SIZING FOR ROTATING BLADES GRIT TANKS

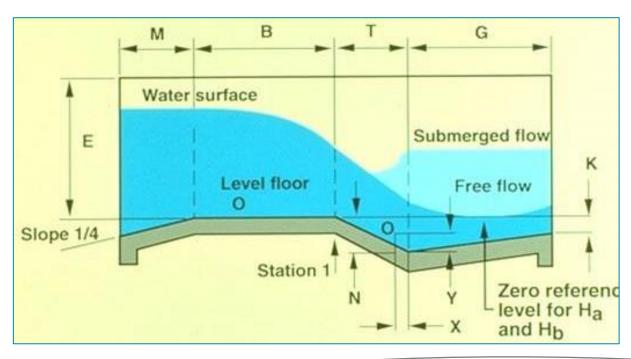
MAIN FEATURES	UNIT	DIMENSIONAL DATA								
MODEL		20	25	30	35	40	45	50	55	60
TANK DIAMETER (d)	mm	2000	2500	3000	3500	4000	4500	5000	5500	6000
BLADES REVOLUTION SPEED	r.p.m.	34	28	26	20	20	17	16	15	13
SEWAGE MAX FLOW RATE	m³/h	150	300	450	600	1000	1250	1850	2200	2650
AIR FOR SAND MIN FLOW RATE	m³/h	60	100	100	100	100	100	150	150	150
SAND WASHING WATER MIN FLOW RATE	m³/h	3,6	3,6	3,6	3,6	7,2	7,2	7,2	7,2	7,2
GEARMOTOR POWER SUPPLY	kW	0,37	0,37	0,55	0,75	1,1	1,5	2,2	3,0	4,0
DIFFUSERS BLOWER POWER SUPPLY	kW	0,37	0,55	0,55	1,1	1,5	1,5	2,2	4,0	4,0
AIR-LIFT BLOWER POWER SUPPLY	kW	3,0	3,0	3,0	5,5	5,5	5,5	7,5	7,5	7,5
WEIGHT	daN	280	300	330	350	380	400	420	440	500





FLUMES

 Known geometry gives a predictable head discharge relationship, measured upstream of the flume, usually via ultrasonics.



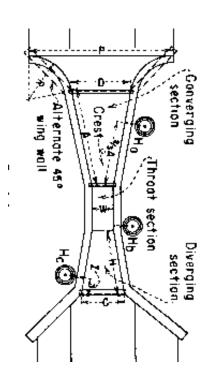






FLUME PARTS

- A flume has three basic parts
 - Entry transition this is where the channel width is reduced to the flume throat width via curved sections.
 The throat should be central to the channel.
 - Throat- this is where the flow passes through the critical depth. The throat length must be at least twice the depth upstream. The throat is usually around half the channel width.
 - Exit transitions this is where the flume throat is widened out to the downstream channel width. This is done using straight tapers.

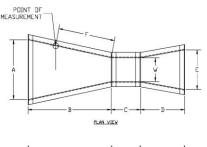


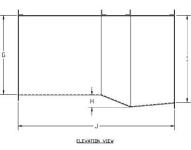




DIMENSIONS & FLOW RANGES

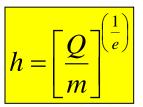
	t Width V)	(cm)								ow hour)	MI			
Inch	(cm)	A	В	С	D	E	F	G	Н	I	J	Minimum	Maximum	
1	2.5	16.7	35.6	7.6	20.3	9.3	24.2	22.9	2.9	24.8	63.5	0.5	19.3	}
2	5.1	21.4	40.6	11.4	25.4	13.5	27.6	22.9	4.3	25.1	77.5	0.7	44.1	
3	7.6	25.9	45.7	15.2	30.5	17.8	31.8	61.0	5.7	63.5	91.4	0.9	115.4	ļ
6	15.2	39.7	61.0	30.5	61.0	39.4	41.4	61.0	10.8	68.6	152.4	5.2	313.9)
9	22.9	57.5	86.4	30.5	45.7	38.1	58.7	76.2	10.8	83.8	162.6	9.3	636.2	<u> </u>
12	30.5	84.5	134.3	61.0	91.4	61.0	91.4	91.4	22.9	99.1	286.7	33.2	1666.2	2
18	45.7	102.6	141.9	61.0	91.4	76.2	96.5	91.4	22.9	99.1	294.3	52.0	2507.5	5
21	53.3	111.6	145.7	61.0	91.4	76.2	96.5	91.4	22.9	99.1	298.1	59.3	2936.5	5
24	61.0	120.7	149.5	61.0	91.4	91.4	101.6	91.4	22.9	99.1	301.9	67.2	3373.5	;
30	76.2	139.1	157.2	61.0	91.4	106.7	106.7	91.4	22.9	99.1	309.6	83.1	4252.0)







PARSHAL FLUME HEAD EQUATION

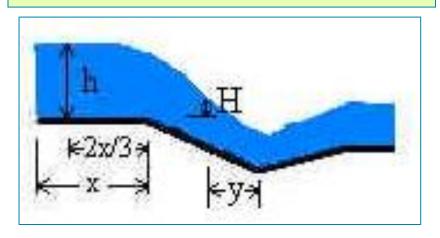


Where:

h : head,ft Q : flow,cfs

e,m: empirical constants dependent

on the throat width



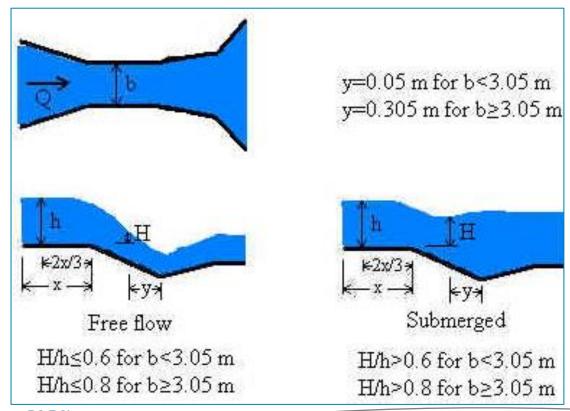
	roat Width N)	e	m
ft	m	Value	Value
0-0.25	0-80	1.550	4xW
0.25-0.5	80-150	1.547	4xW
0.5-0.75	150-230	1.580	4xW
0.75-1	230-300	1.530	4xW
1-1.5	300-460	1.522	4xW
1.5-2	460-610	1.538	4xW
2-3	610-910	1.550	4xW
3-4	910-1220	1.566	4xW
4-5	1220-1520	1.578	4xW
5-6	1520-1830	1.587	4xW
6-8	1830-2440	1.595	4xW
8-10	2440-3050	1.607	4xW
>10	>3050	1.600	3.688xW+2.5





FREE FLOW & SUBMERGED FLUMES

The upstream head must be at least 1.25 times the downstream head. If it is not then the flume is drowned out. This means that the head discharge relationship will no longer be true. The flume will be over recording, I.e. it will indicate that a greater flow has passed than has actually passed.





PRIMARY SEDIMENTATION TANKS(PST)

A tank in which suspended solids are allowed to settle out of a liquid under the influence of gravity.

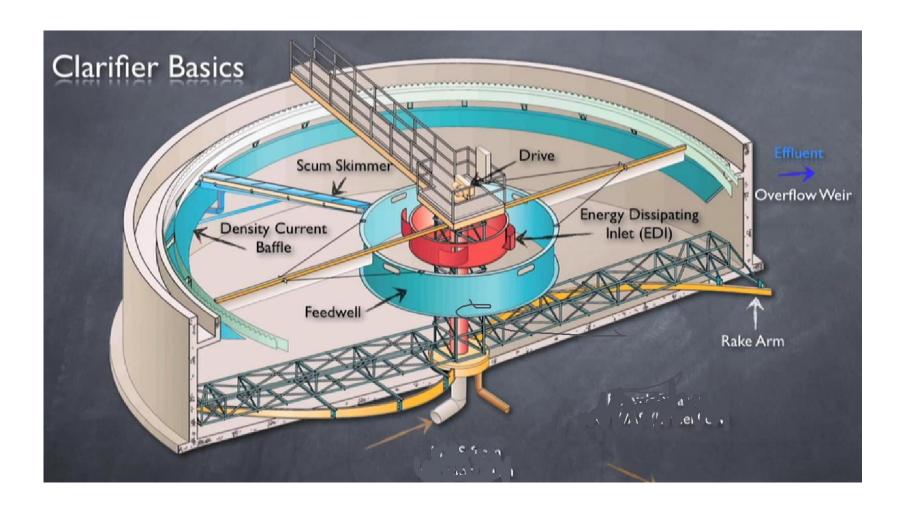
Functions of the primary clarifiers include:

- Remove floating material, thereby minimizing operational issues such as the buildup of scum in the secondary treatment process.
- Concentrate primary sludge before pumping to gravity thickeners, and
- Reduce suspended solids and biochemical oxygen demand (BOD) loading to the downstream treatment processes





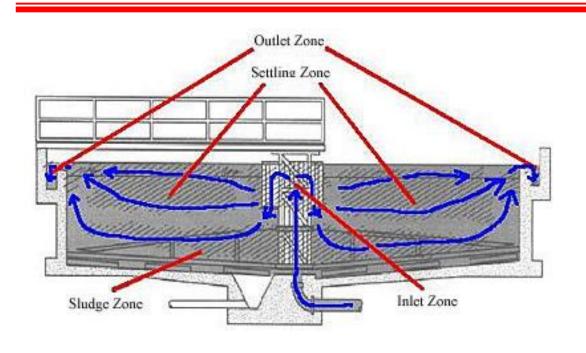
PST COMPONENTS

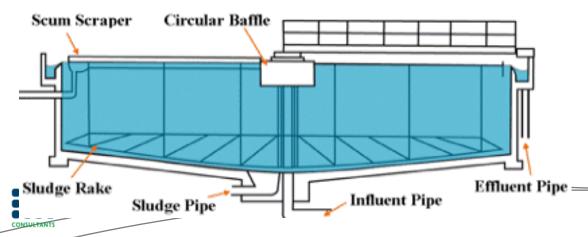






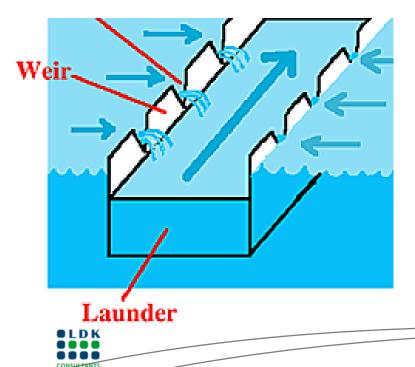
FLOW PATTERN & ZONES IN PSTs





EFFLUENT LAUNDER

Trough which collects the wastewater flowing out of the sedimentation tank and directs it to the effluent pipe. One or both sides of a launder typically have weirs attached. Weirs are walls preventing wastewater from flowing uncontrolled into the launder





TYPICAL DESIGN PARAMETERS FOR PRIMARY SEDIMENTATION TANKS

Item	Unit	PST Foll Secondary	•	PST with Waste Activated Sludge Return		
		Range	Typical	Range	Typical	
Detention Time	hours	1.5-2.5	2	1.5-2.5	2	
Overflow Rate/Surface Loading rate @ Average flow	m³/m².d	30-50	40	24-32	28	
Overflow Rate/Surface Loading rate @ Peak flow	m³/m².d	80-120	100	48-70	60	
Weir Loading	m³/m.d	125-500	250	125-500	250	
Depth	m	3-4.9	4.3	3-4.9	4.3	

Average %TSS removal = 60%





SURFACE LOADING RATE

The surface loading rate is the quantity of wastewater passing over 1 m2 of tank per day

$$SLR = \frac{Flow_Rate}{Tank_Surface_Area}$$

$$Tank_Surface_Area = \frac{Flow_Rate}{SLR}$$





WEIR OVERFLOW RATE

The weir overflow rate is the amount of wastewater leaving the settling tank per linear meter of weir

$$WOR = \frac{Flow_Rate}{Tank_Weir_Length}$$

$$Detention_Time = \frac{Effective_Volume}{Flow_Rate}$$





HYDRAULIC DETENTION TIME

Sufficient time for contact between solid particles is necessary for flocculation and sedimentation.

$$Detention_Time = \frac{Effective_Volume}{Flow_Rate}$$





DESIGN EXAMPLE FOR PST

ltem	Unit	@Qav	@Qpdwf	@Qpwwf
Flow	m3/day	133,900	233,300	295,000
Required Surface Overflow Rate	m3/m2.d	28		
Typical Depth	m	3.5	3.5	3.5
floor slope	deg.	7.5	7.5	7.5
Computed Area based on Qav SLR	m2	4782	4782	4782
No. of Tanks		8	8	8
Area Each	m2	598	598	598
Diameter	m	27.6	27.6	27.6
Used diameter	m	28.0	28.0	28.0
Computed area each tank	m2	616	616	616
Used Total Area	m2	4926	4926	4926
Volume each tank	m3	2155	2155	2155
Calculated Surface loading rate	m3/m2.d	27	47	60
Requied typical SLR	m3/m2.d	28		60
Weir over flow rate @ Qav	m3/m.d	190	332	419
Effective Detention time	hour	3.1	1.8	1.4

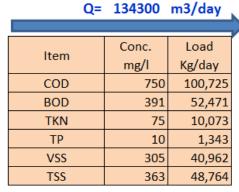


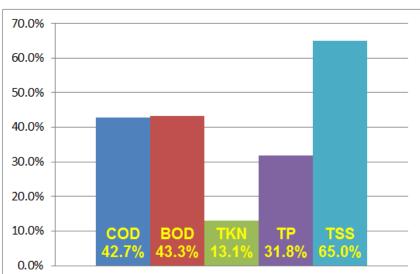


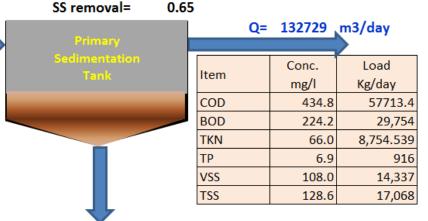


PERCENTAGE POLLUTANTS REMOVAL IN PST

Soluble Particulate 262.0 488.0 133.8 256.9 61.0 14.0 5.2 4.8 305.0 363.1







Q-	13/1	iii3/ uay			
ltem	Conc. mg/l	Load Kg/day	% Removal	Removed Soluble	Removed Particulate
COD	27,378	43,011.6	42.7%	411.6	42600.0
BOD	14,460	22,716.8	43.3%	290.7	22426.1
TKN	839	1,318.0	13.1%	95.8	1222.1
TP	272	427.2	31.8%	8.2	419.0
VSS	16,948	26,625.0	65.0%		
TSS	20,176	31,696.8	65.0%		

PST Removal Rates

m3/day



SWIM-H2020 SM

For further information

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SWIM and Horizon 2020 Support Mechanism

Working for a Sustainable Mediterranean, Caring for our Future

Thank you for your attention.

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