### **SWIM and Horizon 2020 Support Mechanism**

Working for a Sustainable Mediterranean, Caring for our Future

#### **SWIM-H2020 SM Regional Activities 14**

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**SWIM and Horizon 2020 SM** REG-14: Refugee Emergency: Fast track project Design of wastewater

26 March 2018, Beirut, Lebanon

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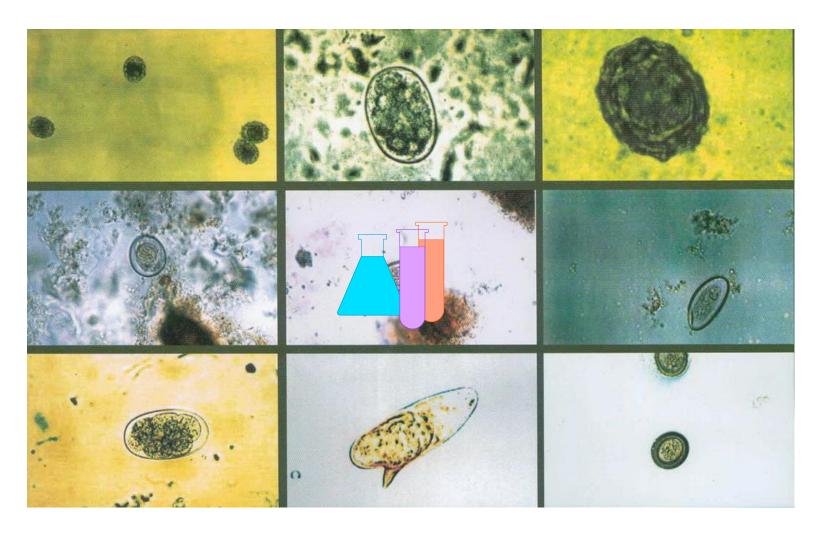








# SESSION -1 PART 2 MICROORGANISMS



### MICROORGANISMS CONTENTS

- 1. Typical Microorganisms in Wastewater
- 2. Classification of Bacteria
- 3. Bacteria Metabolism
- 4. Bacteria growth
- 5. Yield
- 6. Growth kinetic for Nitrification
- 7. Activated sludge kinetic coefficients for Heterotrophic bacteria
- 8. Activated sludge kinetic coefficients for Nitrifying bacteria



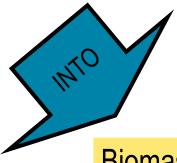


## PURPOSE OF WASTEWATER TREATMENT

**IS TO...** 

### **Transform**

Particulate & Dissolved Organics



Biomass (Primarily Bacterial Bodies)

## Why?



Bacteria Settle

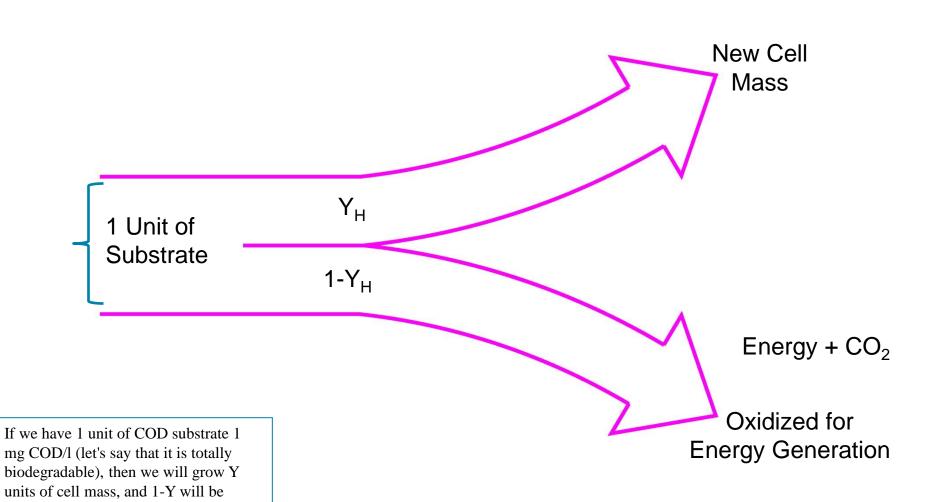


Dissolved Solids Don't



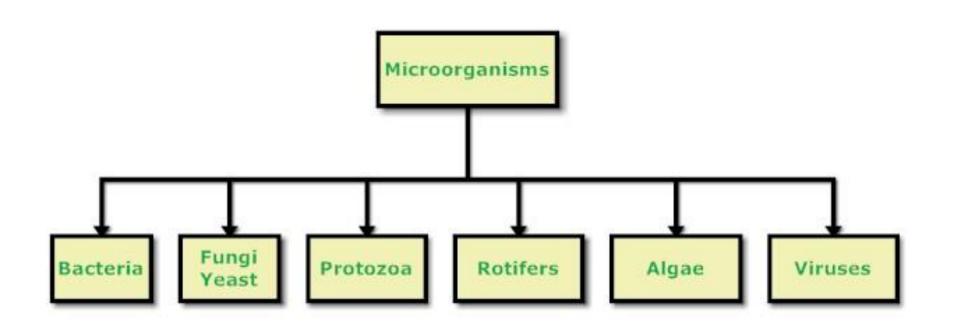


## UTILIZATION OF SUBSTRATE BY HETERETROPHIC ORGANISMS



oxidized for energy.

## TYPICAL MICROORGANISMS IN WASTEWATER







# CLASSIFICATION OF BACTERIA BASED ON NUTRITIONAL REQUIREMENTS

Item	Hetrotrophic Bacteria	Autrotrophic Bacteria		
Energy Source	Organic compounds	Inorganic Compounds		
Carbon Source	Organic compounds	CO <sub>2</sub>		
Types	Aerobic Bacteria	Nitrifying Bacteria		
	Anaerobic Bacteria	Nitrosomonas		
	Facultative Bacteria	Nitrobacter		
		Sulfur Bacteria		





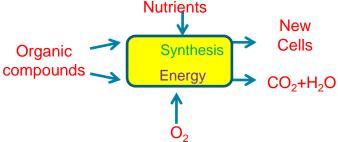
# METABOLISM OF HETEROTROPHIC BACTERIA

- Organic matter is the substrate(food) used as energy source.
- The majority of organic matter in wastewater is in the form of large molecules which can't penetrate the bacteria cell membrane.
- Therefore large molecules are hydrolyzed into diffusible reactions for assimilation into their cells. The first biochemical reactions are hydrolysis of:

Complex carbohydrates sugar units
 Proteins amino acids
 Insoluble fats fatty acids

 Under aerobic conditions the reduced soluble organics compounds are oxidized to end products of CO2 and water.

$$Organics(Aerobic) + O_2 \rightarrow CO_2 + H_2O + energy$$



 Under anaerobic conditions, soluble organics are decomposed to intermediate end products(H<sub>2</sub>S,organic acids) along with production of CO2 water.

$$Organics(Anaerobic) \rightarrow Intermediates + CO_2 + H_2O + energy$$





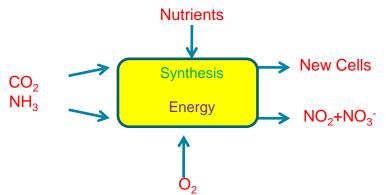
# METABOLISM OF AUTOTROPHIC BACTERIA

 Autotrophic bacteria use CO2 as a carbon source and oxidize inorganic compounds for energy.

Nitrifying Bacteria

$$NH_3 + O_2 \xrightarrow{Nirosomona \ s} NO_2^- + energy$$

$$NO_2^- + O_2 \xrightarrow{\text{Nitrobacte } r} NO_3^- + energy$$



Sulfur Bacteria

$$H_2S + O_2 \rightarrow H_2SO_4 + energy$$

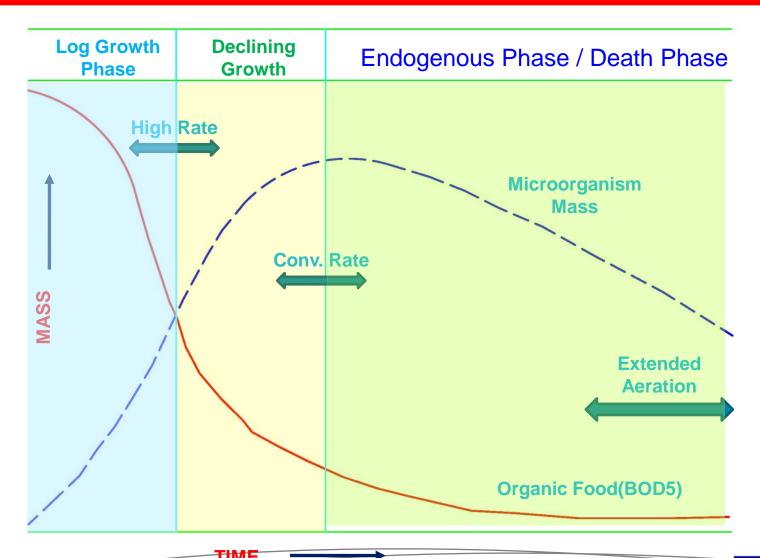
Iron Bacteria

$$Fe^{2+} + O_2 \rightarrow Fe^{3+} + energy$$



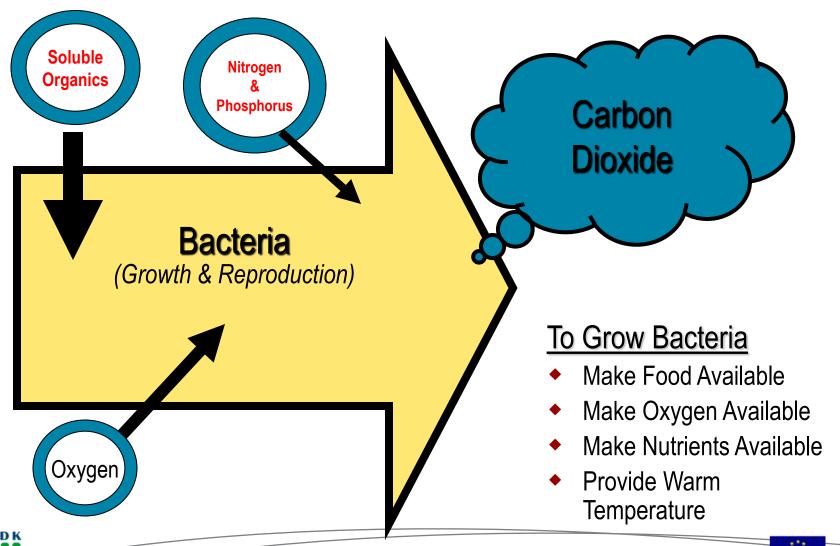


## **BACTERIAL GROWTH PATTERNS**

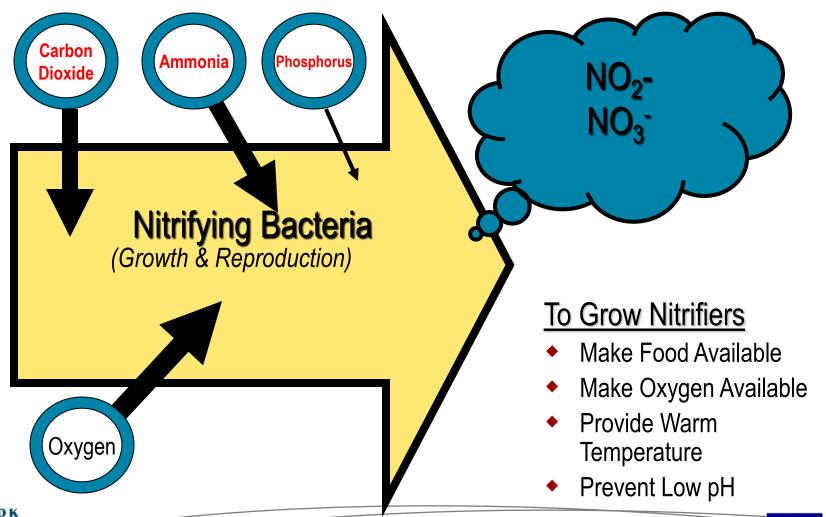




## HETEROTROPHIC BACTERIAL GROWTH



## **NITRIFIRES GROWTH**



## **DEFINITIONS & TERMINOLOGY**

#### Substrate

Carbon source (organic and inorganic)

#### Heterotrophs

- Organisms that use organic carbon to produce new cells.
  - e.g. most organisms used in aerobic treatment of wastewater

#### Autotrophs

- Organisms that use CO2 to produce new cells.
  - e.g. Nitrifying bacteria

#### Nutrients

- Essential For Growth and Maintenance Of Micro-organisms
- e.g. Macro nutrients (N and P). Micro nutrients (Metals such as Fe, Ca, Mg, K, Mo, Zn, Co)





## **Definitions & Terminology**

## Mixed Liquor(ML) & Mixed Liquor Suspended Solids(MLSS)

- ☐ ML ,Mixture of wastewater and microorganisms(bugs) in the aeration tank.
- ☐ MLSS ,concentration of bugs in the mixed liquor.

#### Microorganisms(Bugs)

☐ Microscopic living objects which require energy, carbon and small amount of inorganic elements to grow and multiply. They get these requirements from the wastewater and the sun and in doing so help to remove the pollutant from wastewater

#### Nitrification

☐ Nitrification is the biological oxidation of ammonia with oxygen into nitrite followed with the oxidation of these nitrites into nitrates.

#### Denitrification

□ The reduction of nitrate or nitrite to gaseous products such as nitrogen, nitrous oxide, and nitric oxide; brought about by denitrifying bacteria.

#### Lysis

☐ To separate, breakdown of a cell often by viral, enzymic or osmotic by rupture of the cells wall.





## **MICROBIAL GROWTH KINETICS**



## **BACTERIAL METABOLISM**

- The metabolic activity of bacteria is the primary means of removing pollutants in a bioreactor. Estimating production of biomass is a key step in the analysis and design of activated sludge system in general and bioreactor in particular and involve two aspects:
  - Kinetics, which deals with rates of bacterial growth and decay reactions(how fast the reactions will occur)
  - Stoichiometry, which deals with reactions and relationships between the masses of reactants and products involved in the reactions.
- Reactions affecting biomass production are:
  - Bacterial growth from uptake of substrate.
  - Bacterial loss from decay or endogenous respiration.





## STOICHIOMETRY SYNTHESIS (TRUE) YIELD

Synthesis or true yield(Y,) is a stoichiometric parameter that
is generally defined as the mass of biomass produced per
unit mass of biodegradable substrate consumed. This
represents the "true yield", applies only to the biodegradable
fraction of the substrate and active biomass produced, and
doesn't account for the effect of biomass decay.

$$Y = \frac{Biomass\_Produced}{Substrate\_Re\ moved} = \frac{\mu_{max}}{k}$$



Y = synthesis or true yield.

k = maximum specificsubstrate utilization rate.

µmax = maximum specific growth rate,1/d



Kinetic Coefficients





#### **NET BIOMASS YIELD**

The net biomass yield( $Y_{net}$  or  $Y_{bio}$ ) is different than the "true yield", it is defined as the ratio of net biomass growth rate to the substrate utilization rate. It includes biomass decay. It is used to estimate the amount of active microorganisms in the system.

$$Y_{net} = \frac{Net\_bio\_mass\_production\_rate}{substrate\_utilization\_rate}$$

$$Y_{net} = \frac{-r_g}{r_{su}}$$

$$Y_{net} = \frac{production\_rate - decay\_rate}{substrate\_utilization\_rate}$$

$$Y_{net} = \frac{Y}{1 + k_d \times SRT}$$

#### Where

et = net biomass yield, g biomass (AVSS)/ g substrate used.





## **OBSERVED YIELD**

The observed yield Y<sub>obs</sub> is based on the actual measurement of the amount of solids production relative to the substrate removal.

$$Y_{obs} = \frac{Total\_MLVSS\_Production\_Rate}{Substrate\_removal\_Rate}$$

$$Y_{obs} = \frac{P_{X,VSS}}{Q(S_o - S)}$$

$$Y_{obs} = \frac{P_{X,TSS}}{Q(S_o - S)}$$

#### Where

Y<sub>obs</sub> = observed yield, g VSS produced/g substrate removed.

g TSS produced/g substrare removed.

 $P_{X,VSS}$  = net waste activated sludge produced, kg VSS/day.

 $P_{X,TSS}$  = net waste activated sludge produced, kg TSS/day.

Q = Average influent flow

 $S_0$  = influent substrate concentration (mg/l)

= effluent substrate concentration (mg/l)





## **STOICHIOMETRY**

- Most simulation models base all calculations of organic material(including biomass) on COD.
- For practical purposes biomass has to be expressed as suspended solids.
- It is estimated that 1 gram of volatile suspended solids is equal to 1.42 gram of COD. This is based on the assumption that the composition of a typical bacterial cell(biomass) can be characterized as C<sub>5</sub>H<sub>7</sub>NO<sub>2</sub>.

$$C_5H_7NO_2 + 5O_2 \rightarrow 5CO_2 + 2H_2O + NH_3$$

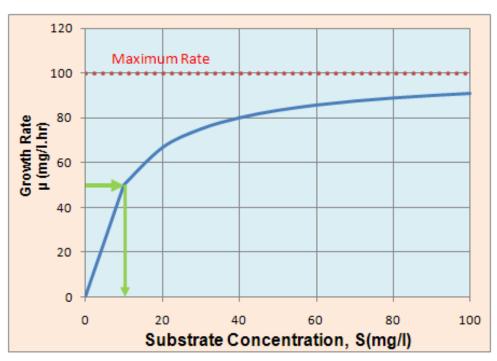
 This implies that 160 g of oxygen are required(COD) to completely oxidize 113 g of biomass(VSS). Thus the COD/VSS ratio is 160/113=1.42





## HALF-VELOCITY CONSTANT (K<sub>S</sub>)

 The half-velocity constant is the value of the soluble substrate concentration at an one-half the <u>maximum specific substrate</u> <u>utilization rate</u>..



- The relationship developed by Monod(1949) forms basis for bacterial growth kinetics.
- Rate of bacterial growth and substrate utilization is a function of the concentration of the limiting substrate(e.g. BOD or NH3) surrounding the bacteria and the concentration of active bacteria.

Kinetic Coefficients





## EFFECT OF TEMPERATURE ON KINETIC COEFFICIENTS

$$k_T = k_{20} \times \theta^{(T-20)}$$

#### Where

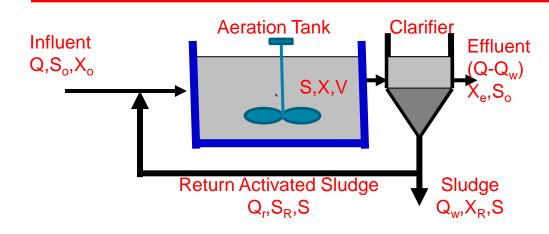
 $k_T$  = reaction rate coefficient at temperature T, °C.

 $k_{20}$  = reaction rate coefficient at 20 °C.  $\theta$  = temperature coefficient(1.02-1.25).

T = temperature, °C.



#### **EFFLUENT DISSOLVED SUBSTRATE CONCENTRATION**



$$S = \frac{K_S [1 + k_d SRT]}{SRT(Yk - k_d) - 1}$$

$$\mu_m = k Y$$

$$S = \frac{K_S [1 + k_d SRT]}{SRT(\mu_m - k_d) - 1}$$

S

- The effluent soluble substare concentration for a complete mix activated sludge process is only a function of the SRT and kinetic coefficients for growth and decay.
- The effluent substrate concentration is not related to the influent soluble substrate concentration.
- The influent concentration affects the biomass concentration.

Where:

s : effluent soluble substrate concentration g
 BOD or bsCOD/m3

SRT: sludge age

 $\mu_m$  = maximum specific growth rate,1/d.

K<sub>s</sub>: Half-velocity constant

k<sub>d</sub>: endogenous decay coefficient, g VSS/gVSS.d

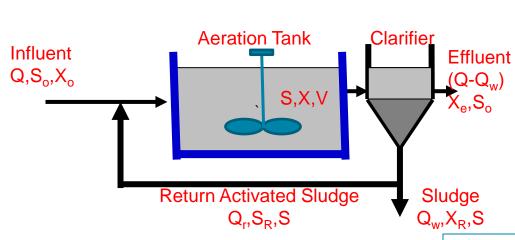
Y: True yield heteretrophs.

: Maximum specific substrate utilization rate





#### BIOMASS CONCENTRATION IN THE AERATION TANK



$$X = \left(\frac{SRT}{\tau}\right) \left[\frac{Y(S_o - S)}{1 + k_d SRT}\right]$$

$$\tau = \frac{V}{Q}$$

$$X = \left(\frac{SRT}{V}\right) \left[\frac{YQ(S_o - S)}{1 + k_d SRT}\right]$$

The reactor biomass concentration is function of:

- SRT
- Aerobic detention time.
- Yield coefficient
- Amount of substrate removed(S-S<sub>o</sub>).

#### Where:

X: Biomass concentration, g/m3

SRT: sludge age

 $k_d$ : endogenous decay coefficient, g VSS/gVSS.d

Y: True yield heterotrophs, mg VSS/mg BOD or

COD

S<sub>o</sub>: Influent soluble substare concentration g BOD

or bsCOD/m3

S : Effluent soluble substarte concentration, BOD

or bsCOD/m3.

 $\tau$ : hydraulic detention time, V/Q, day.



# DECAY (LOSS OF BIOMASS) CELL DEBRIS(ENDOGENOUS PRODUCTS)

- VSS in the bioreactors include:
  - Active biomass.
  - nbVSS in the influent wastewater.
  - Cell debris.
- Cell debris
  - The remaining non-biodegradable material after cell death and lysis.
  - Cell wall is non-biodegradable and contribute to the cell debris.
  - Cell debris represents about 10 to 15 percent of the original cell weight.
- The rate of production of cell debris is directly proportional to the endogenous decay rate.

$$r_{XD} = f_d \times k_d \times X$$

Cell Debris Calculator

#### Where:

r<sub>XD</sub> = rate of cell debris production, g VSS/m3.d

f<sub>d</sub> = fraction of biomass that remains as cell debris(0.10-0.15 g VSS/g VSS)

k<sub>d</sub>: endogenous decay rate, g VSS/gVSS.d

X = Active biomass concentration mg/l



### **TOTAL VOLATILE SUSPENDED SOLIDS**

Total Volatile suspended solids = Biomass production

+ nbVSS from cell debris

+ nbVSS in influent





## **ACTIVE BIOMASS(AVSS) FRACTION**

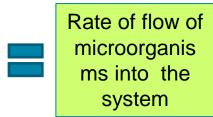
$$F_{AVSS} = \frac{Net\_Biomass\_Production(growth - decay)}{MLVSS}$$





## MODELLING SUSPENDED GROWTH TREATMENT PROCESSES BIOMASS MASS BALANCE

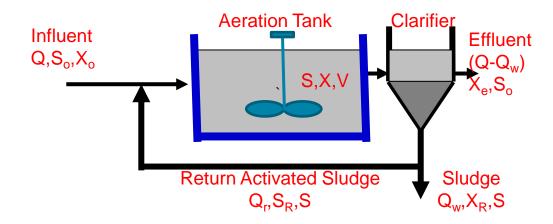
Rate of accumulation of microorganisms within the system



Rate of flow of microorganisms out of the system



Net growth of microorganisms







## **GROWTH KINETICS FOR NITRIFICATIONS**

$$\mu_n = \mu_{nm} \times \frac{N}{K_N + N} - k_{dn}$$

Assuming excess DO is available

$$\mu_{n} = \mu_{nm} \times \frac{N}{K_{N} + N} \times \frac{DO}{K_{O} + DO} - k_{dn}$$

Accounts for DO concentration

#### Where

 $\mu_n$  = specific growth rate of nitrifying bacteria, g new cells/g cells.d

 $\mu_{nm}$  = maximum specific growth rate of nitrifying bacteria, g new cells/g cells.d

N = nitrogen concentration, g/m3.

K<sub>n</sub> = half-velocity constant for ammonia concentration, substrate concentration at one half the maximum specific substrate utilization rate, g/m3.

k<sub>dn</sub> = endogenous decay coefficient for nitrifying organisms, g VSS/g VSS.d.

DO = DO concentration

K<sub>O</sub> = half-velocity constant for DO concentration





#### SWIM-H2020 SM

#### For further information

Website

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### **SWIM and Horizon 2020 Support Mechanism**

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### Thank you for your attention.

This Project is funded by the European Union





























## **Appendix**





#### MAXIMUM RATE OF SOLUBLE SUBSTRATE UTILIZATION (k)

- This coefficient is used for designing a <u>complete-mix activated-sludge system</u> and has to do with the biomass growth process. Substrate in biological processes used for wastewater treatment, referrers to the organic matter or nutrients in wastewater, that are converted during biological treatment or that may be limiting in biological treatment.
- In specific circumstances, there will be a certain rate with which the soluble substrate will be depleted by bacteria. At a high substrate concentration, the utilization rate will be high and will be practically even to the maximum rate of soluble substrate utilization

$$\mu_m = kY$$







## ACTIVATED SLUDGE KINETIC COEFFICIENTS FOR HETEROTROPHIC BACTERIA-METCALF & EDDY FOURTH EDITION

Coefficient		Unit	Value @ 20 °C		Temp. Correction (θ Value)	
			Range	Typical	Range	Typical
Maximum specific bacterial growth rate	μ <sub>m</sub>	gVSS/g VSS.d	3-13.2	6	1.03-1.08	1.07
Half-velocity constant	K <sub>s</sub>	mg BOD/I	25-100	60	1	1
		mg bsCOD/I	10-60	40	1	1
		mg bCOD/I	5-40	20	1	1
True yield /Synthesis yield coefficient)	Y	mgVSS/mg BOD	0.4-0.8	0.6		
		mgVSS/mg bCOD	0.3-0.5	0.4		
Endogenous decay coefficient	<b>k</b> <sub>d</sub>	g VSS/g VSS.day	0.06-0.2	0.12	1.03-1.08	1.04
Cell debris fraction	f <sub>d</sub>	Unitless	0.08-0.2	0.15		





## COMPARISION OF TYPICAL KNETIC COEFFICIENTS FOR AEROBIC OXIDATION OF BOD

Parameter		Unit	Metcalf & Eddy/AECOM Fifth Edition		Metcalf & Eddy Fourth Edition	
			Range	Typical	Range	Typical
Maximum specific substrate utilization rate	k	b bsCOD/g VSS.d	4-12	6	2-10	5
Half-velocity constant	Ks	mg/l BOD	20-60	30	25-100	60
		mg/l bsCOD	5-30	15	10-60	40
True yield /Synthesis yield coefficient)	Y	mg VSS/mg BOD	0.4-0.8	0.6	0.4-0.8	0.6
		mg VSS/mg COD	0.4-0.6	0.45	0.3-0.6	0.4
Endogenous decay coefficient	b,kd	g VSS/g VSS.d	0.06-0.15	0.1	0.06-0.15	0.1





### **ACTIVATED SLUDGE KINETIC COEFFICIENTS FOR NITRIFYING BACTERIA**

Coefficient		Unit	Value @ 20 °C		Temp. Correction (θ Value)	
			Range	Typical	Range	Typical
Maximum specific growth rate of nitrifying bacteria	$\mu_{mn}$	gVSS/g VSS.d	0.2-0.9	0.75	1.06-1.123	1.07
Half-velocity constant for ammonia concentration	K <sub>n</sub>	mg NH4-N/I	0.5-1	0.74	1.06-1.123	1.053
Biomass true yield /Synthesis yield coefficient)	Y <sub>n</sub>	mgVSS/mg NH4-N	0.1-0.15	0.12		
Endogenous decay coefficient for nitrifying organisms	$\mathbf{k}_{dn}$	g VSS/g VSS.day	0.05-0.15	0.08	1.03-1.08	1.04
Half-velocity constant for dissolved -oxygen concentration	K <sub>o</sub>	mg/l	0.40-0.60	0.5		







